

# **Environmental Compliances in Thermal Power Plant**

## **- Issues & Challenges**

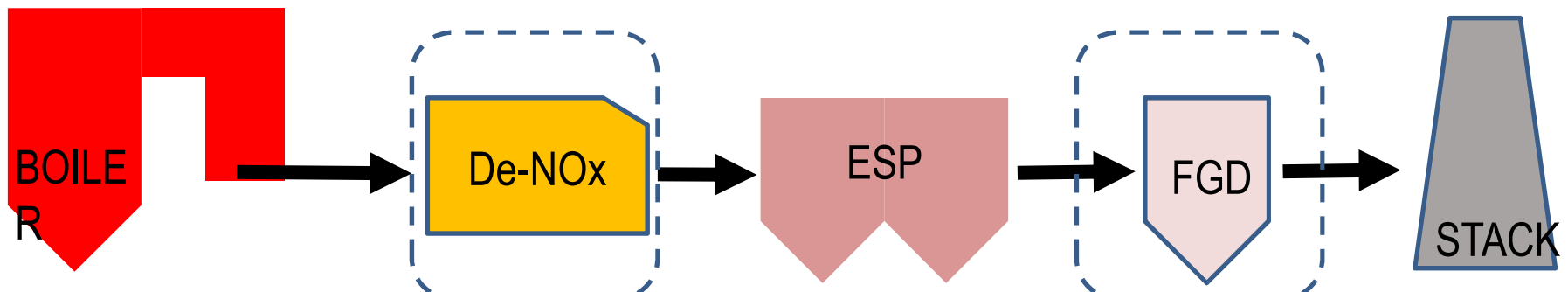
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# Changes in Environment Norms : A Challenge

Old Norms		New Norms				
<i>All emission are in mg/ Nm<sup>3</sup></i>		Installed before 31.12.2003		Installed after 01.01.2004 & up to 31.12.2016		Installed after 01.01.2017
Unit Size	All	< 500 MW	≥ 500 MW	< 500 MW	≥ 500 MW	All
SO <sub>2</sub>	Dispersion through Chimney	600	200	600	200	100
NOx	No Norms	600		300		100
SPM	100	100		50		30
Mercury	No Norms	--	0.03	0.03		0.03



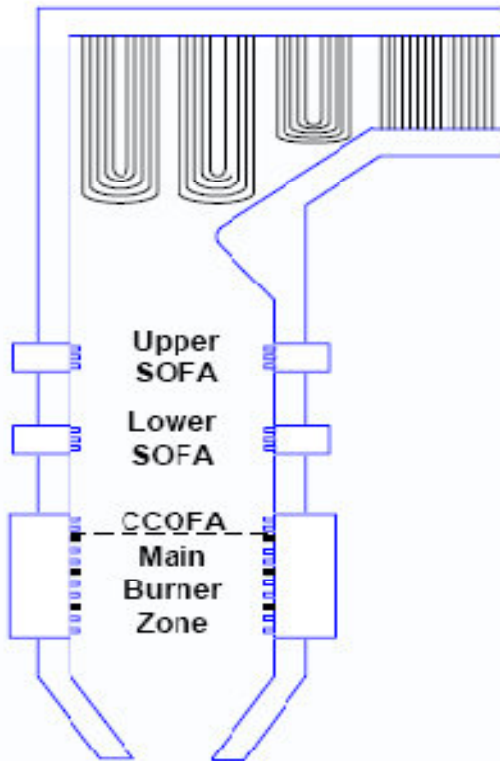
# **Available Technology Options for Emission Control**

# DeNOx Technologies

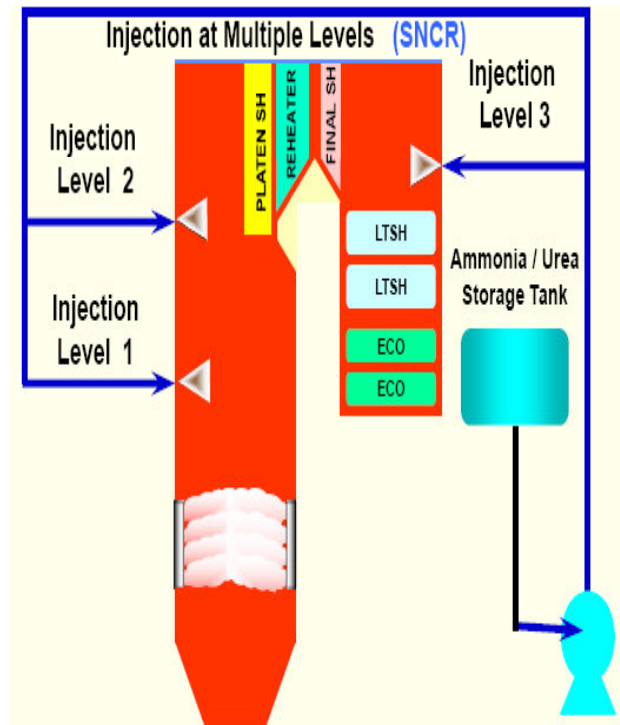
Available Technology	In Combustion	Post Combustion	
	Combustion Modification	Selective Non Catalytic eReduction (SNCR)	Selective Catalytic Reduction (SCR)
Variants & measures to control NOx	Low NOx Burner, Windbox modification, Various type of over fire air	Reagent: Anhydrous/Aqueous Ammonia OR Urea	Catalyst type: Plate/ Honeycomb Reagent: Anhydrous/ Aqueous Ammonia or Urea
Reduction Efficiency	20 – 60 %	25-40 %	90 % & Above
Installation Cost	Low	Moderate	High
Operational Cost	None	High (manly reagent cost)	High (Aux power, reagent cost & catalyst replacement)
Process of NOx reduction	Staging of combustion air	<p><b>Using NH<sub>3</sub></b></p> $4\text{NO} + 4\text{NH}_3 + \text{O}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$ <p><b>Using Urea</b></p> $4\text{NO} + 2\text{CO}(\text{NH}_2)_2 + \text{O}_2 \rightarrow 4\text{N}_2 + 4\text{H}_2\text{O} + 2\text{CO}_2$	$4\text{NO} + 4\text{NH}_3 + \text{O}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$ $2\text{NO}_2 + 4\text{NH}_3 + \text{O}_2 \rightarrow 3\text{N}_2 + 6\text{H}_2\text{O}$
Temperature required	NA	870° to 1100°C	300° to 400°C

# DeNOx Technologies

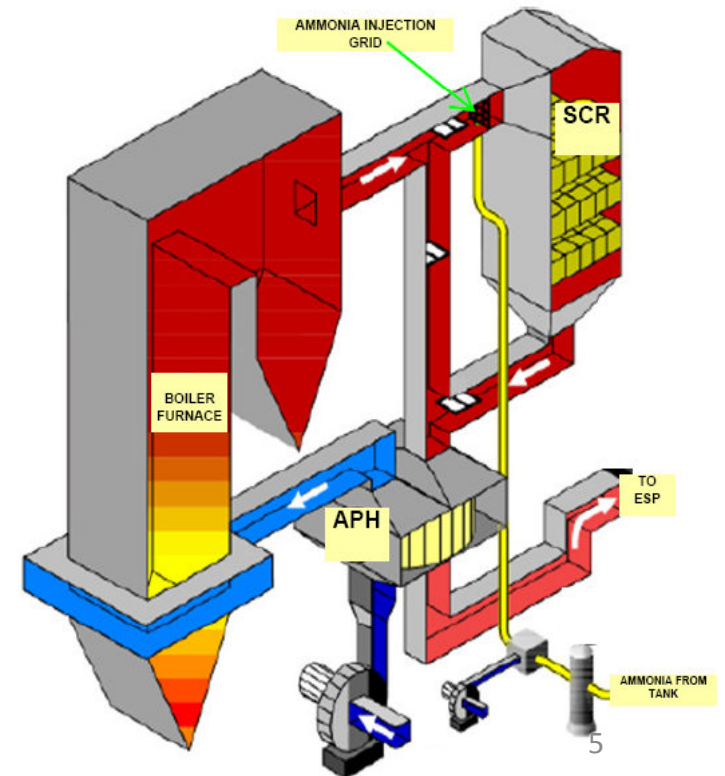
## Combustion Modification



## Selective Non-Catalytic Reduction (SNCR)



## Selective Catalytic Reduction (SCR)



# SCR Catalyst Deactivation

- **Poisoning** by chemical attack (Arsenic, Phosphorus, Heavy Metals)
- **Masking** of catalyst surface by ash
- **Plugging** of catalyst surface pores by fine ash particles
- **Sintering** causing alteration of catalyst pore structure (due to exposure to high temperatures beyond 450°C)

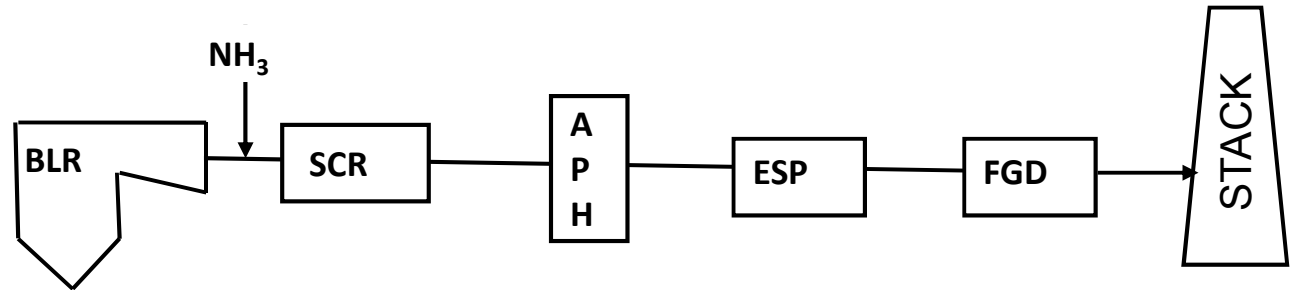


# SCR Catalyst Erosion

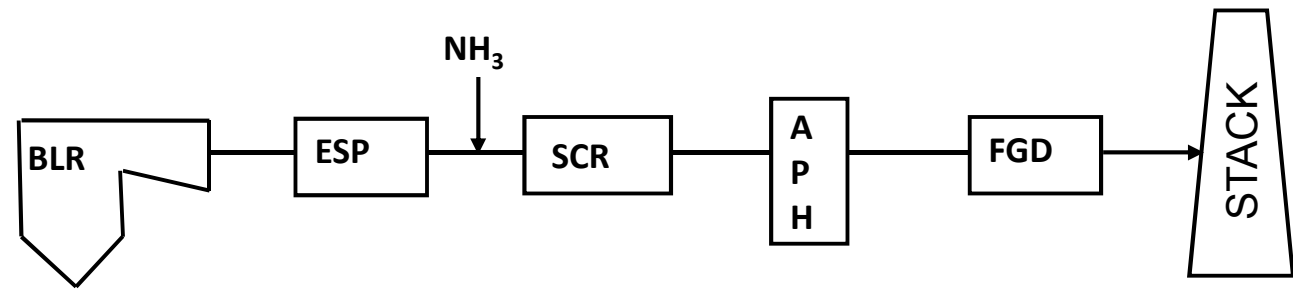
- **High ash**
- **Erosive Content of Ash** (Silica + Alumina, typically > 85% for Indian coal ash)
- **Ash particle size and shape**
- **Plugging susceptibility of catalyst**

# Possible SCR Configuration to deal with high ash

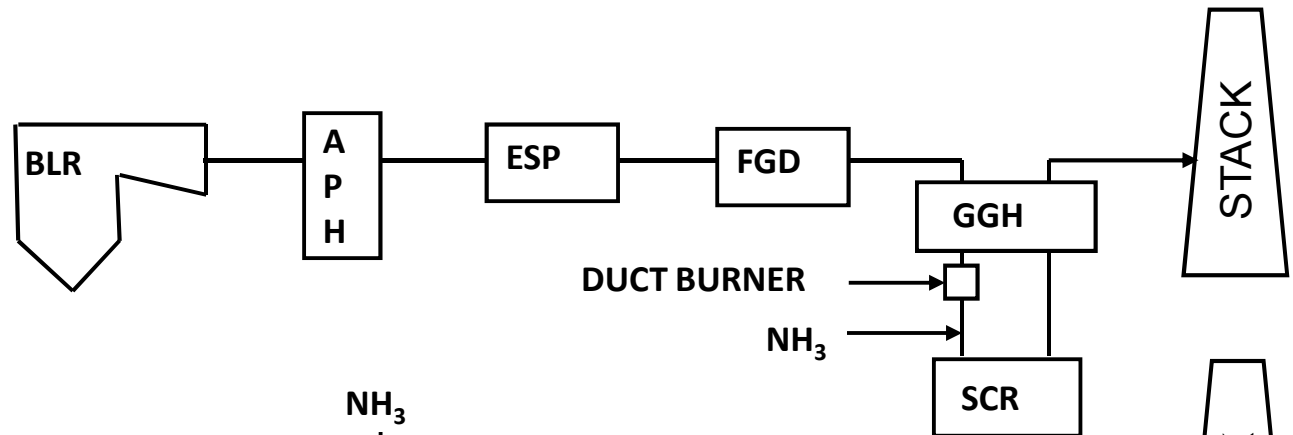
High Dust SCR



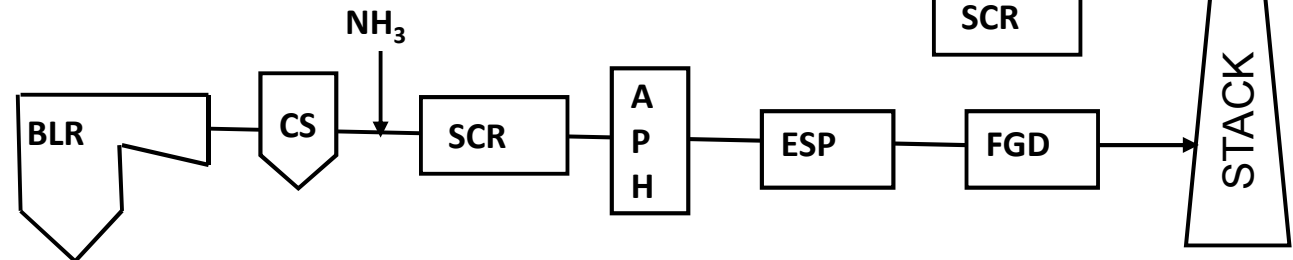
Low Dust SCR, Hot ESP



Lowest Dust, Cold End SCR



Low Dust SCR





# DeNOx Technologies

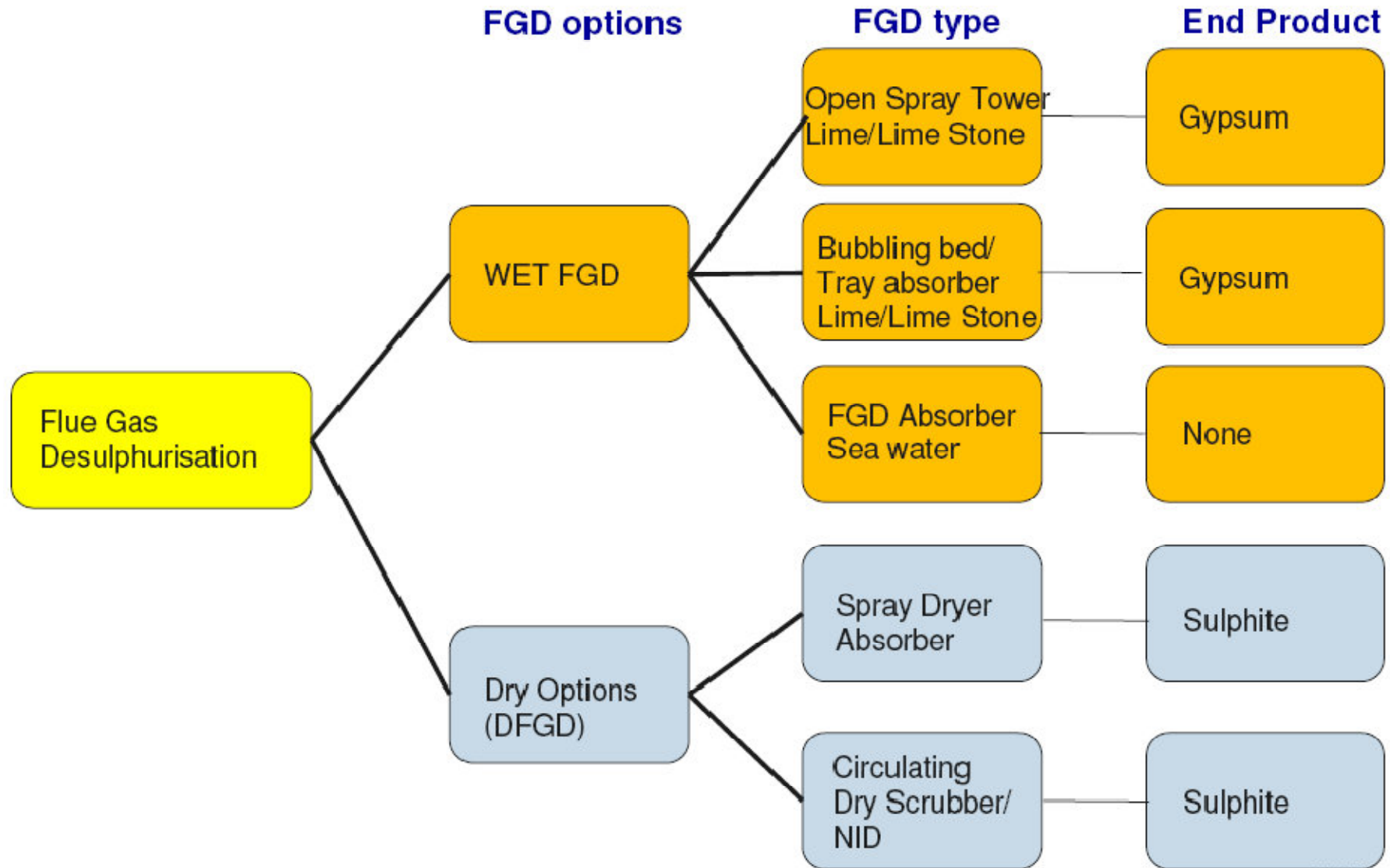
## Challenges

- DeNOx technology is yet to be established for high and erosive ash coals
- Technology proven only upto dust load of 30-40 gm/Nm<sup>3</sup> against our requirement of 80-90 gm/Nm<sup>3</sup>
- SCR catalyst is and extremely fast moving highly expensive item (life expectancy 2.5 - 3 yrs)
- Very limited SCR catalyst suppliers worldwide, none in India

## Way Forward

- A cautious approach needs to be adopted rather than embarking upon hurriedly
- Pilot slip stream tests with India coals will provide quick learning opportunity both to the manufacturers as well as the plant operators
- Cyclone dust separators upstream of SCR could be a good approach to start with
- Rapid indigenization of catalyst manufacturing a must for long term sustenance

# DeSOx Technologies



# DeSOx Technologies

Parameters	WET Limestone FGD	DRY FGD (SDA/CDS/NID)
Commercially Available Range	~ 1,100 MWe	~ 300-400 MWe single absorber.. For NID each module of 75 MWe
SO <sub>2</sub> removal efficiency	Upto 99 %	up to 99 % (90-95 % for SDA)
Installation Cost (ZLD & Chimney lining cost incl.)	High	Low
Operating Cost	Moderate	High
Sorbent	CaCO <sub>3</sub> (limestone)	CaO / Ca(OH) <sub>2</sub>
Sorbent costs (Rs/ton)	~ 2000	~ 6000
Water consumption	1.0 with GGH 1.4 without GGH	0.7
Auxiliary Power Consumption	High with GGH Moderate without GGH	Moderate
Flue gas temperature at FGD outlet	Saturation temperature 50 – 60 °C (Without GGH)	75 – 85 °C
SO <sub>3</sub> removal	< 40 %	> 98 %
Condition of existing stack	Existing stack to be modified in all cases	Existing stack can be used without modification

# DeSOx Technologies

Parameter	WET Limestone FGD	DRY FGD (SDA/CDS/NID)
<b>FGD by-product disposal</b>	Gypsum is produced which is saleable when limestone purity is > 90%. & emission from ESP < 50 mg/Nm <sup>3</sup>	Product for disposal (CaSO <sub>3</sub> /CaSO <sub>4</sub> ). Space required for disposal
<b>Waste water</b>	Waste water generated which needs to be treated for Zero liquid discharge (ZLD)	Waste water free system and can also utilise waste water from other sources.
<b>Erection period</b>	~ 30 Months	~ 24 Months

# Limestone Factsheet

- Production of limestone in India is around 300 MTPA
- Cement companies account for 50% of limestone production and mostly have their own captive mines.
- Majority of limestone is of 80%-85% purity which will produce gypsum for cement or fertiliser but not for gypsum board.
- Current Gypsum rates vary between Rs 700-1200 per Ton.
- *Limestone mines are distributed almost all over India.*
- High quality limestone (purity > 90%) is mostly available in Rajasthan

# DeSOx Technologies

## Challenges

- Wet DeSOx technologies are relatively more matured yet new to majority of Indian operators
- Wet limestone based FGD, although a preferred option, has large consumptive water requirement associated with extremely polluted blow down which must be taken care through an expensive ZLD system
- Lime stone supply and gypsum off take chain needs to be evolved quickly
- FGD retrofit may not be possible in many of the older stations

## Way Forward

- No major issues in adoption in new units

# Chimney Material for Retrofit Cases

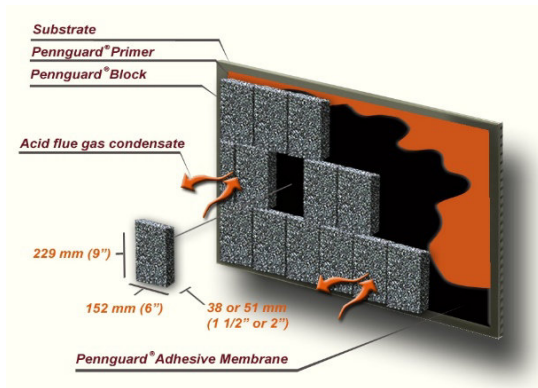
ITEM	BOROSILICATE GLASS BLOCKS	GLASS FLAKE REINFORCED VINYL ESTER COATING
THICKNESS	51 MM	1.5 MM
SERVICE TEMPERATURE	UPTO 199 DEG C CONTINUOUS	UPTO 140 DEG C CONTINUOUS
DESIGN LIFE	30 YEARS	8-10 YEARS
GUARANTEE LIFE	10 YEARS	3-4 YEARS
COST	VERY HIGH	LOW
SUPPLIERS	HADEK, NETHERLANDS ECOCERA, KOREA	AKZONOBEL, JOTUN, DENSO, CORROCOAT, HEMPEL, STEULLER
APPLICATOR	LOCAL APPLICATOR TRAINED BY SUPPLIER	AUTHORIZED APPLICATORS
EXECUTION TIME	2-3 MONTHS	2-3 MONTHS

# Chimney Material for New Builds

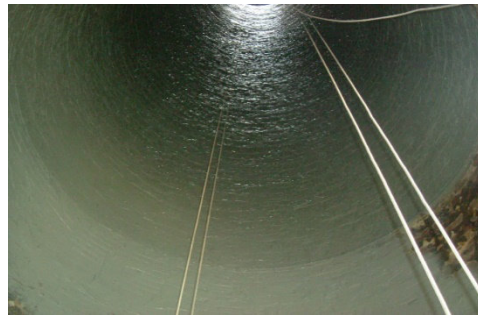
ITEM	FRP FLUE LINER	Titanium Clad Sheet
THICKNESS	25MM	1.2 MM Ti+ 10 MM MS
SERVICE TEMPERATURE	UPTO 150 DEG C CONTINUOUS	UPTO 900 DEG C CONTINUOUS
DESIGN LIFE	30 YEARS	20 YEARS
GUARANTEE LIFE	3 YEARS	-
COST	LOW	HIGH
SUPPLIERS	PLASTICON, DENMARK FIBROGRATS, INDORE	CHINESE SUPPLIERS
APPLICATOR	AUTHORIZED APPLICATORS	FABRICATION IS COMPLEX. DATA NOT AVAILABLE
EXECUTION TIME	6-8 MONTHS	6-* MONTHS



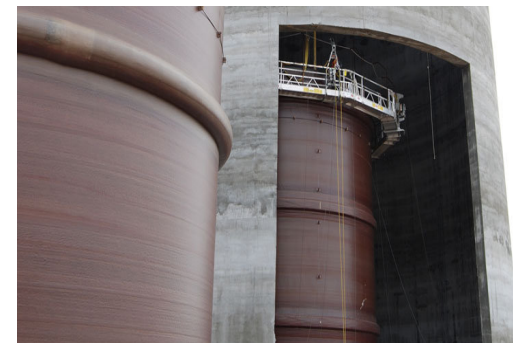
## Borosilicate Glass



## Flake Glass Coating



## FRP Flue Liner



# Mercury Emission Control

- Globally, there is no mature / commercially available technology for mercury emission control
- Fortunately, India coals have relatively lower mercury content (0.5 ppm)
- The other emission control measures like FGD and ESP by default capture a significant portion of mercury

# Closed Cycle Cooling - Implications

## Inland Project Retrofits

- Higher consumptive water requirement due to higher evaporation losses
- Reduced power generation efficiency due to higher cooling water temperature by around 2%.
- Serious layout constraints within acquired land limits

## Coastal Projects

- Coastal projects are endowed with abundance of saline sea water and should be permitted to employ open cycle cooling for better efficiency (lower emissions)
- Sea water FGD is the least cost option for deSO<sub>x</sub> which will be completely ruled out if open cycle cooling is not permitted

# Reduced Water Consumption

(2.5m<sup>3</sup>/Hr/MW)

- Typically 2.1m<sup>3</sup>/Hr/MW of water is lost in closed cycle cooling from the cooling towers
- Limestone based wet FGD consumes about 0.25 m<sup>3</sup>/Hr/MW of water
- In addition, there are evaporation and seepage losses from bottom ash dyke
- Hardly any water left for other consumptive needs
  - DM water consumption
  - Potable water
  - Fugitive coal and ash dust suppression
  - Green belt and plant horticulture

# Summary

- Promulgation of new environment norms by MoEF is a commendable move
- The emission norms are comparable with the best in the world
- However, in order to make implementation of the norms more practicable and better feasible, it is suggested that
  - Older units which have already lived half their life or more may be exempted from retrofits due to various technical constraints
  - Emission control technologies are still in developmental stage, especially for Indian coals, at least 5 – 7 years should be allowed for compliance
- NTPC is committed to implement all of the stipulations in the units ordered after issuance of the new norms (07.12.2015).

*Thank You*